



Multi-{physics, phase, scale} computational modeling of interface-coupled problems in redox flow batteries

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Background

- Redox flow batteries (RFBs) are gaining prominent attention for addressing the urgent need of deploying large-scale energy storage technologies to integrate intermittent renewables.
- RFBs have interesting features including higher durability and power-energy decoupling.
- Large-scale deployment of RFBs has feasibility issues regarding costs and efficiency.
- Coupled multi-scale computational models can accelerate our understanding of intricate RFB processes, providing a unique perspective to guide the design of RFB components.

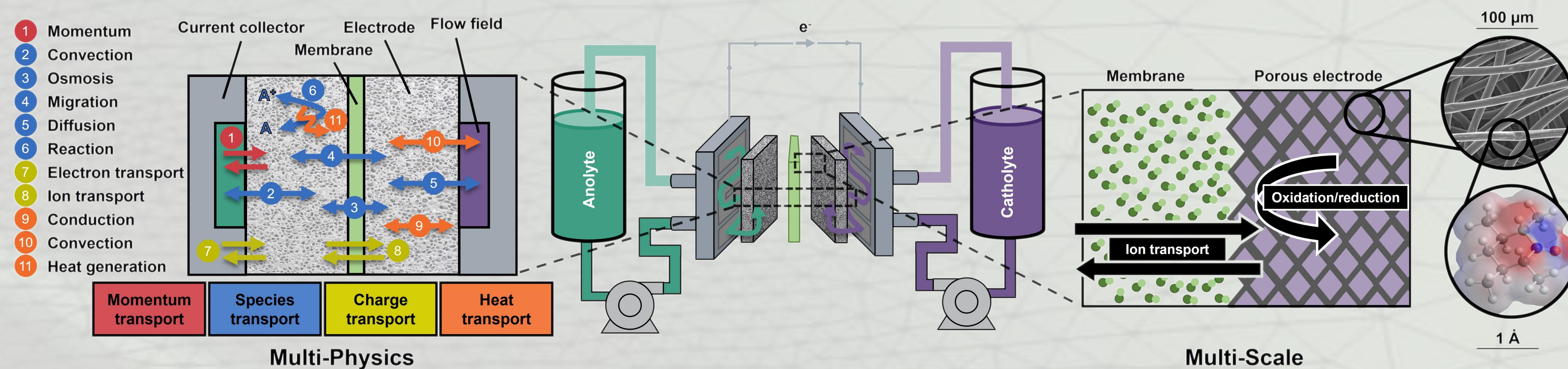


Fig 1: In RFBs, electrolyte solution containing dissolved or suspended active species is stored in external tanks and pumped through the electrochemical stack where the active species undergo electrochemical reactions to charge/discharge the battery.

Methodology

- In this research, we are developing multi-{physics, phase, scale} models of the RFB processes.
- These processes range from transport phenomena on the cell level to the microstructure effects on the pore-scale.
 - Macro-scale:** Finite element/volume methods to solve electrochemical reactions equations.
 - Meso-scale:** Lattice Boltzmann method (LBM) for the flow through the porous electrode.
 - Nano-scale:** Density functional theory (DFT) to model the kinetic rates of reactants.

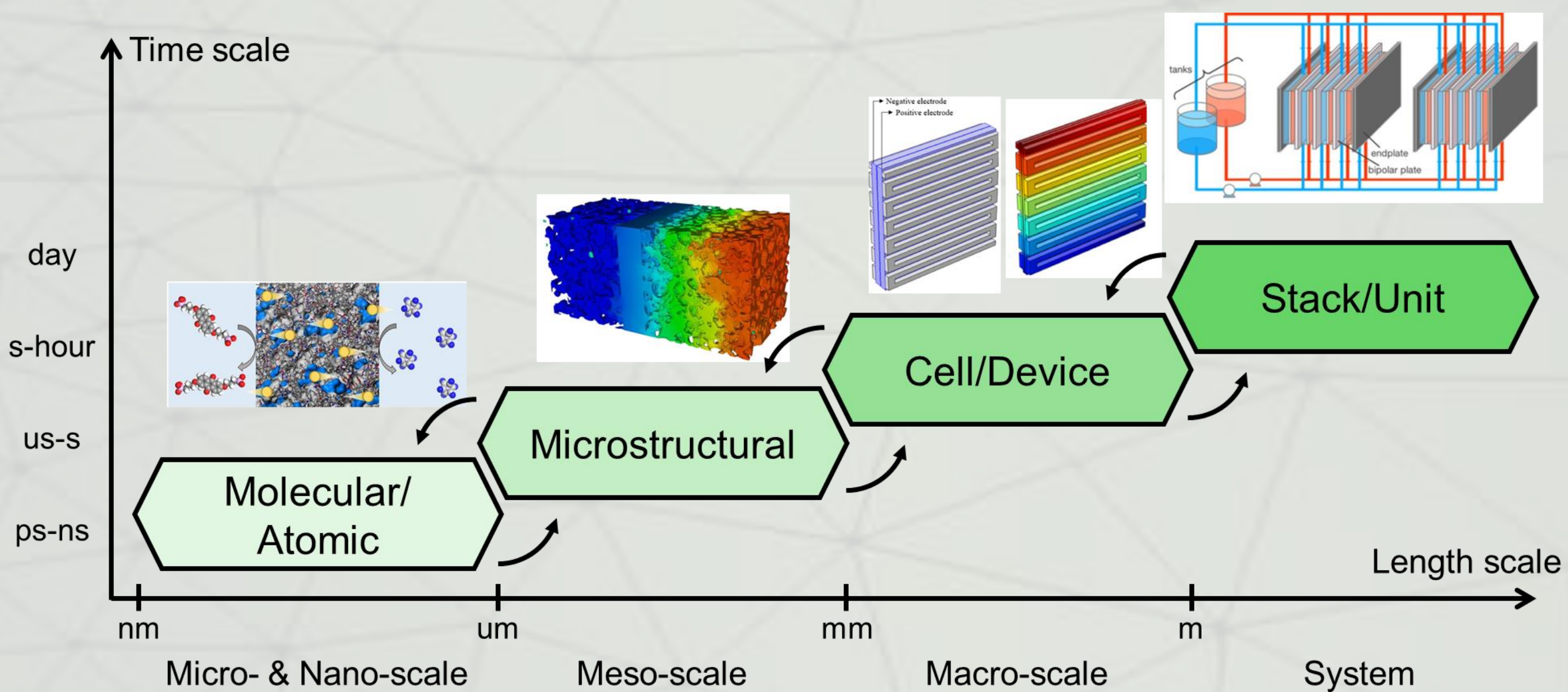


Fig 2: Various time and length scales in RFBs (figures adapted from [1-4]).

Meso-scale

- Pore-scale simulations are essential to understand how pore shape and transport impact the RFB performance.
- LBM excels in handling complex multi-phase phenomena and high-performance computing, making it suitable for pore-scale simulations when a high resolution is required.

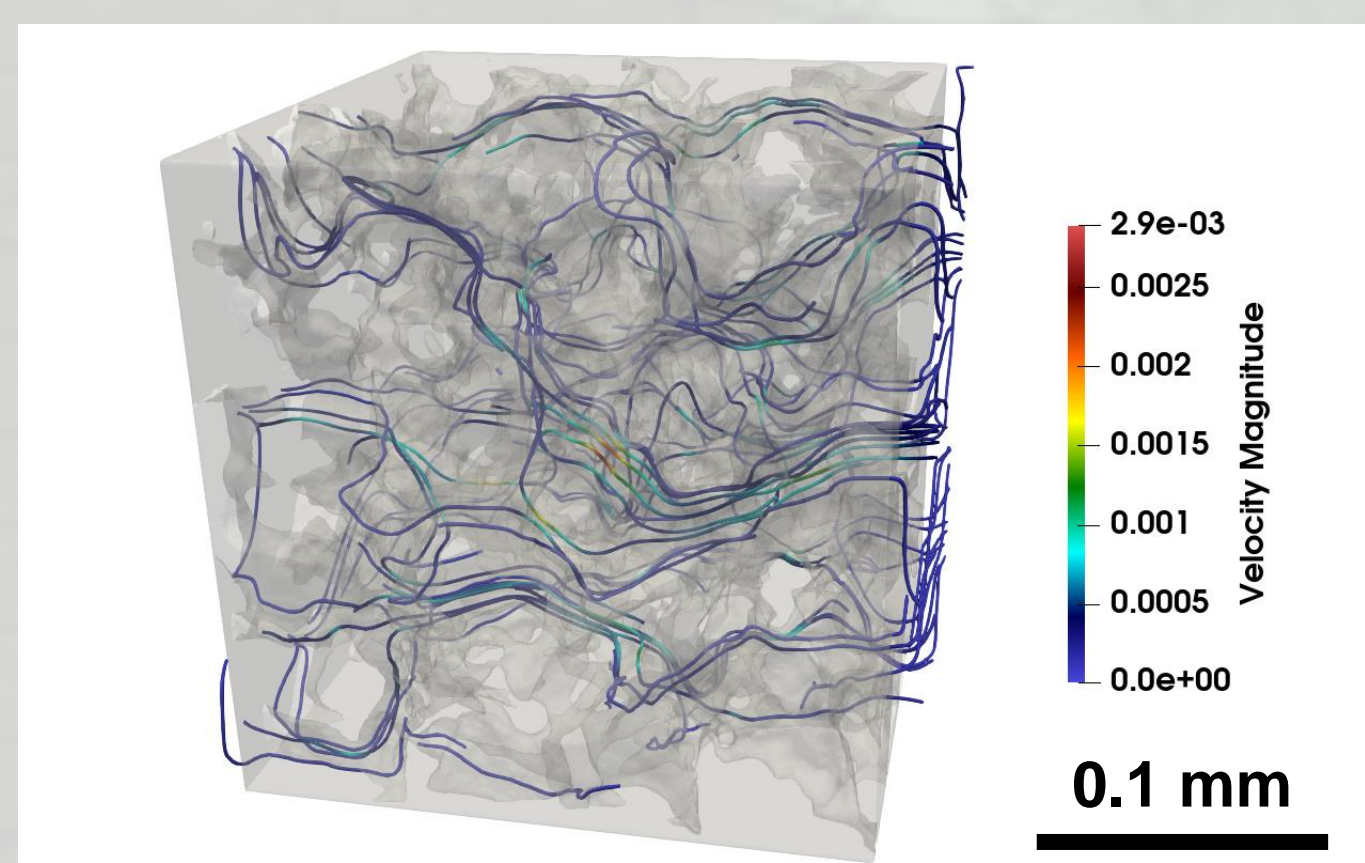


Fig 3: Single-phase simulation of flow inside a porous electrode. Colors show the magnitude of the velocity field plotted over the streamlines.

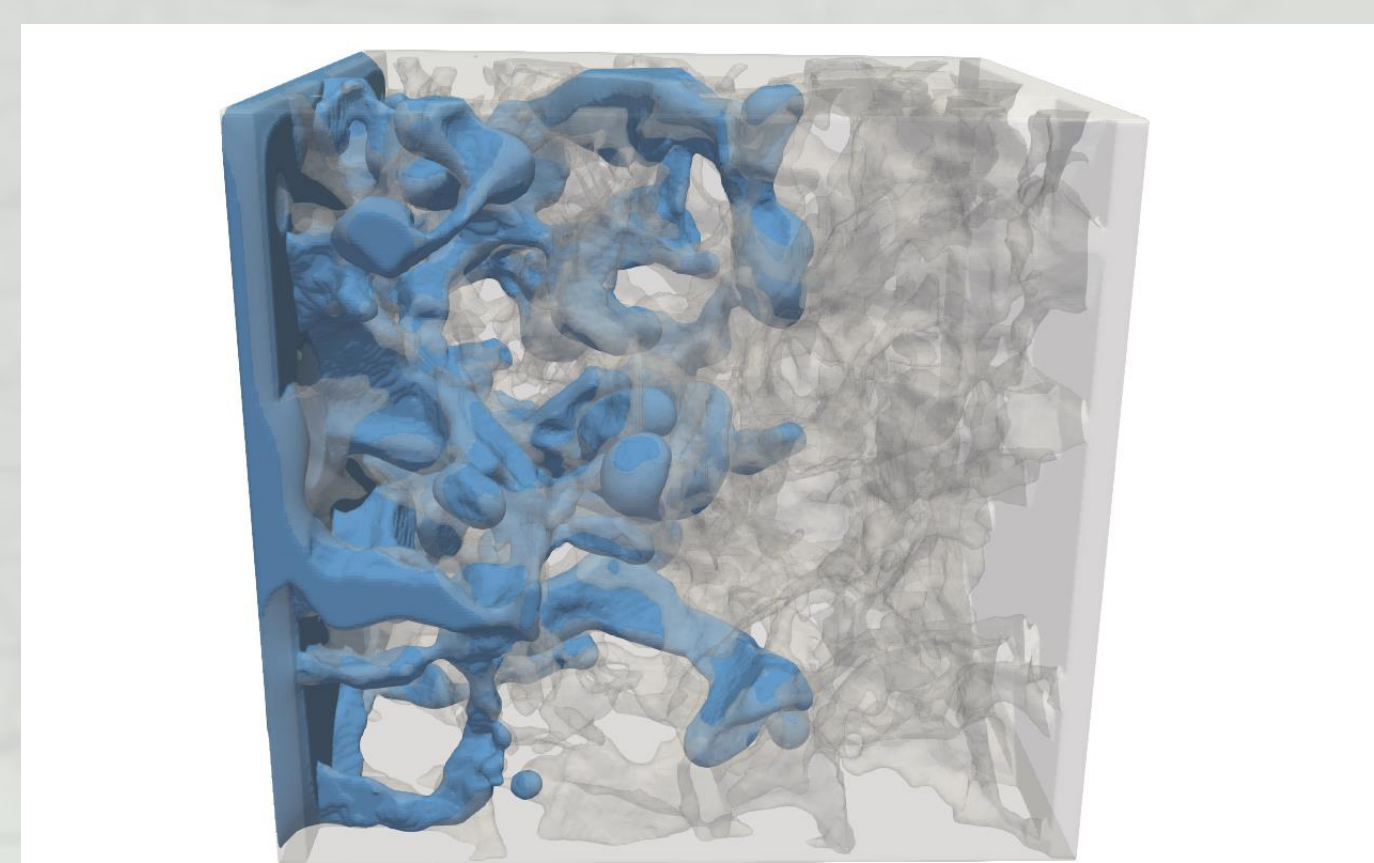


Fig 4: Multi-phase simulation of flow inside a porous electrode, where first phase (plotted in blue) removes and replaces the second phase (not plotted).

Macro-scale

- Macro-scale transport equations provide insights into how reactor design influences RFB performance, which can be simulated by high-performance numerical methods applied to the entire reactor setup's computational mesh.

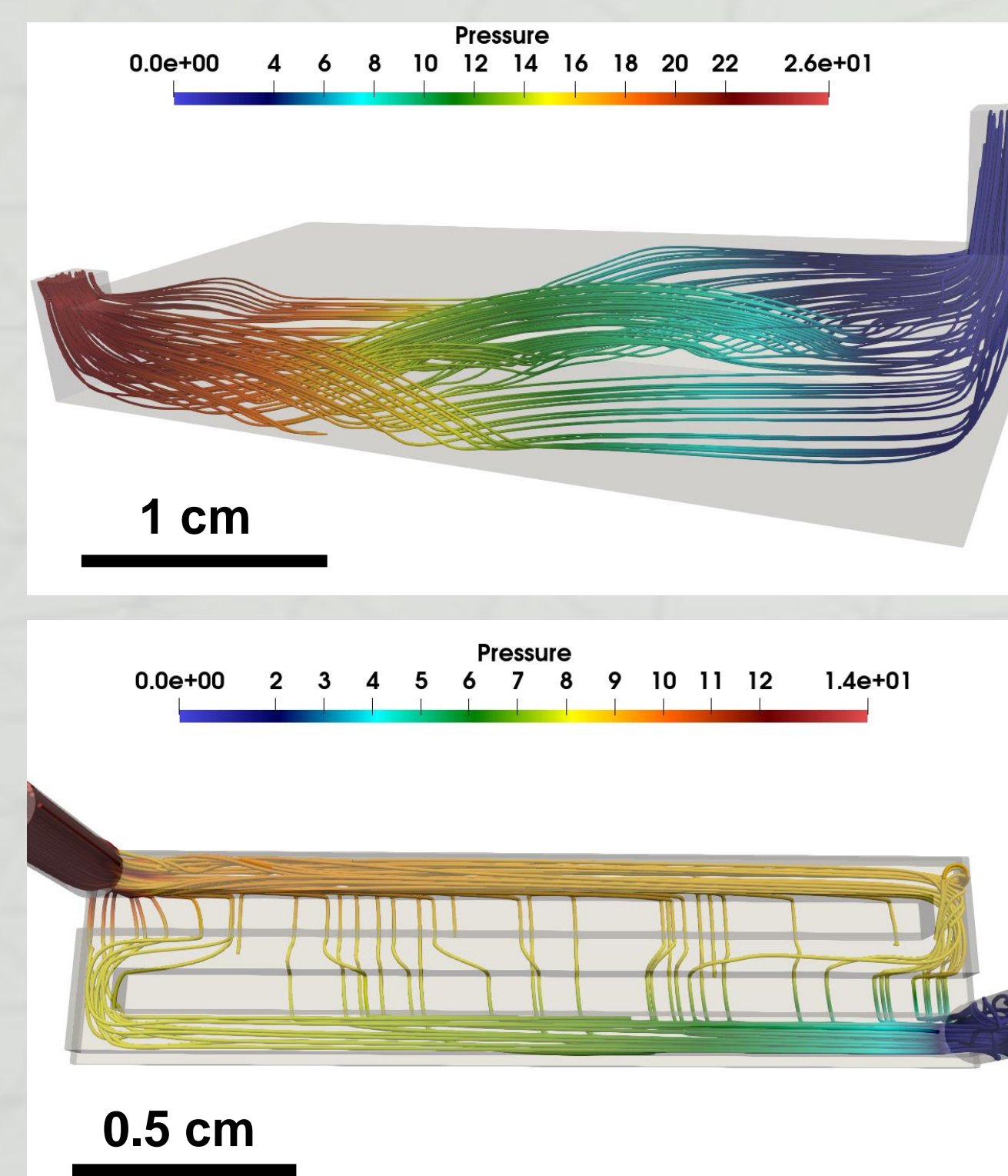


Fig 5: Flow simulation inside a porous electrode represented as a solid block with variable porosity (inlet on the left and outlet on the right). Colors demonstrate the reference pressure drop plotted over the streamlines of the velocity field.

Fig 6: Flow simulation inside a half-cell setup of an RFB, in which the flow field (fluid channel) is positioned on top a porous electrode modeled by Darcy equation. Colors show the reference pressure drop plotted over the streamlines.

Acknowledgements

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References

- [1] Ye et al., *Angew. Chem.*, 61 (2023) e202207580.
- [2] De Lauri et al., *ACS Appl. Energy Mater.*, 4 (2021) 13847.
- [3] Ali et al., *J. Energy Storage*, 28 (2020) 101208.
- [4] Ma et al., *J. Electrochem. Soc.*, 165 (2018) A2209.